

Heat loss through exhaust gases for steam and hot water boilers

TI010

Version 2 (09/12)

$$qA = \frac{f}{CO_2max} \cdot \frac{21}{21 - O_2} \cdot (t_A - t_L)$$

- qA = waste gas loss in %, in relation to the firing capacity and lower calorific value
- f = factor according to the table below
- CO₂ max. = maximum carbon dioxide content (Vol. %) according to the table below
- O₂ = measured oxygen content in Vol. % in dry exhaust gas
- t_A = measured exhaust temperature °C
- t_L = reference and combustion air temperature 25 °C (constant)

If only the carbon dioxide content in the dry exhaust gas is measured, the following conversion applies:

$$O_2 = 21 \cdot \left(1 - \frac{CO_2}{CO_2max}\right)$$

- O₂ = calculated oxygen content (Vol. %) in the dry exhaust gas which has to be used in the formula for determining the heat loss
- CO₂ = measured carbon dioxide content in Vol. % in the dry exhaust gas
- CO₂ max. = maximum carbon dioxide content in Vol. % according to the table below

For the following factors and fuels, it is possible to determine the waste gas loss with a precision of 0.2%.

| Fuel | CO ₂ max Vol. % | Siefert Factors f as function of the O ₂ -content in Vol. % | | | | |
|--|-------------------------------|--|--------|--------|--------|--------|
| | | 1.91 | 2.74 | 3.50 | 4.20 | 4.85 |
| Nat. gas L (Hu = 8.83 kWh/m ³ n) | 11.67 | 0.4721 | 0.4677 | 0.4628 | 0.4608 | 0.4568 |
| Nat. gas H (Hu = 10.35 kWh/m ³ n) | 11.94 | 0.4764 | 0.4720 | 0.4681 | 0.4644 | 0.4609 |
| Fuel oil EL (Hu = 11.89 kWh/kg) | 15.31 | 0.5885 | 0.5841 | 0.5808 | 0.5755 | 0.5737 |
| Heavy oil SA (Hu = 11.22 kWh/kg) | 16.00 | 0.6202 | 0.6163 | 0.6133 | 0.6091 | 0.6062 |
| Propane (Hu = 25.89 kWh/m ³ n) | 13.69 | 0.5295 | 0.5253 | 0.5206 | 0.5183 | 0.5145 |
| Propane-Butane (Hu = 27.95 kWh/m ³ n) | 13.78 | 0.5326 | 0.5282 | 0.5242 | 0.5210 | 0.5175 |
| Butane (Hu = 34.39 kWh/m ³ n) | 14.00 | 0.5406 | 0.5361 | 0.532 | 0.5289 | 0.5253 |
| Nat. gas GZ 35 (Hu = 7 kWh/m ³ n) | 11.12 | 0.4610 | 0.4569 | 0.4524 | 0.4494 | 0.4465 |
| Nat. gas GZ 41,5 (Hu = 8 kWh/m ³ n) | 11.67 | 0.5213 | 0.5166 | 0.5113 | 0.5090 | 0.5045 |
| Nat. gas GZ 50 (Hu = 9 kWh/m ³ n) | 11.67 | 0.4631 | 0.4589 | 0.4541 | 0.4513 | 0.4481 |
| Gas oil HL Schwechat (Hu = 11.64 kWh/m ³ n) | 15.72 | 0.6041 | 0.6000 | 0.5952 | 0.5916 | 0.5898 |
| Gas oil CLU 3 (Hu = 11.4 kWh/m ³ n) | 16.11 | 0.6094 | 0.6056 | 0.6016 | 0.5993 | 0.5956 |
| Biogas (70% Methane) (Hu = 6.97 kWh/m ³ n) | 16.00 | 0.6759 | 0.6694 | 0.6635 | 0.6579 | 0.6529 |
| Biogas (50% Methane) (Hu = 4.98 kWh/m ³ n) | 20.95 | 0.9496 | 0.9404 | 0.9321 | 0.9241 | 0.9170 |

Interim values are to be interpolated.



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Example:

Fuel nat. gas H, measured oxygen content 3,41 Vol %

$$f = 0,4720 + \frac{0,4681 - 0,4720}{3,50 - 2,74} \cdot (3,41 - 2,74)$$

- In Germany, Technical Information TI002 applies for monitoring of the compliance of waste gas losses in boilers covered by the Federal Emissions Protection Act.
- Area of validity of the formulae: without waste gas condensation, waste gas temperature from 50 to 350 °C.
- Under EN 12953 part 11 (shell boilers - Acceptance tests) section 8.3 the reference temperature is a constant 25 °C. In contract to the Fed.Em.Prot.Act formula, the combustion air temperature does not affect the waste gas loss.
- The precise factors in the formulae for waste gas losses were worked out on the basis of EN 12953 p art11 (large capacity boilers acceptance tests) and simplified to give the above easy-to-use formulae.
- The above equation for heat loss through waste gases corresponds to I (N)G according to equation 8.6-1 in EN 12953 part 11. The index N relates to the lower calorific value (Net Calorific Value NCV).